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Full paper available in proceedings
of copper 2022

Hydrogen reduction of entrapped metal oxides from fayalitic copper slags

Gunnar Hovestadt
Bernd Friedrich

Special thanks to Florian Wegmann

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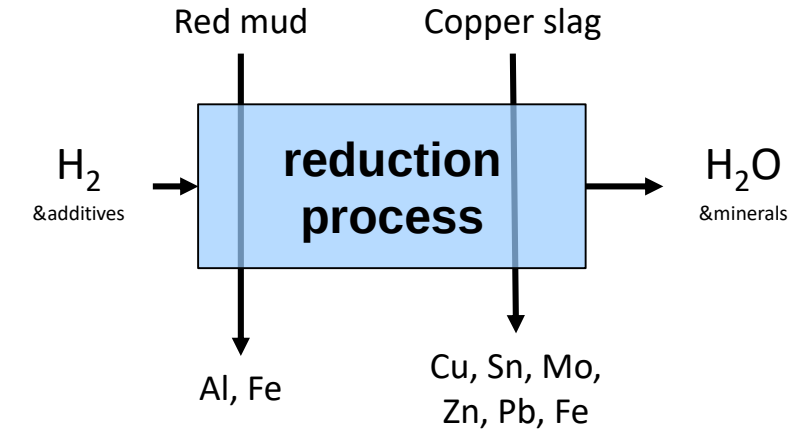
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European project **HARARE**

- Demonstrate H₂-reduction for non-ferrous residues
- Laboratory to industrial scale
- Full process concept
 - Thermochemical simulation
 - Reduction processes
 - By-product evaluation and metal separation
 - LCA and economical study



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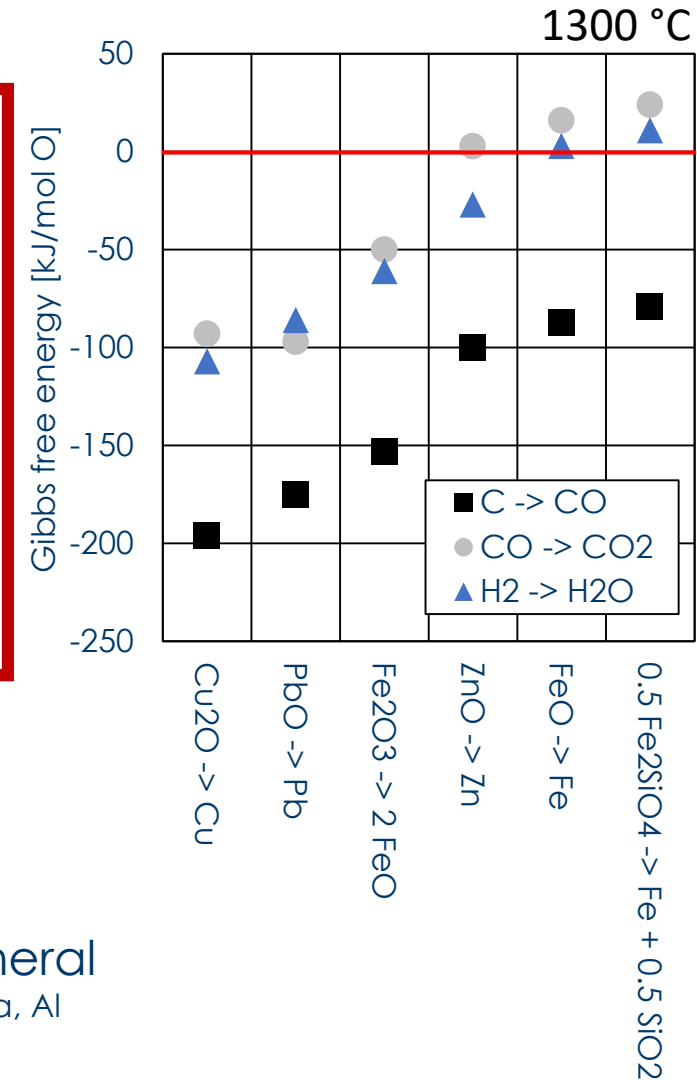
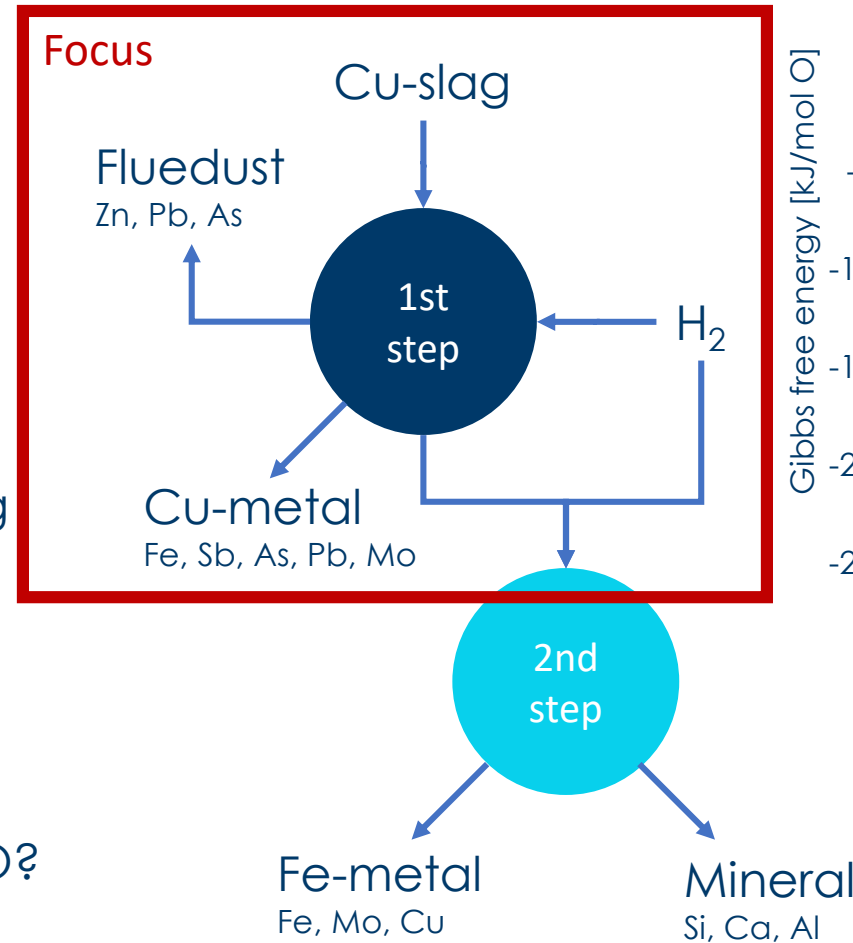
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Flow sheet of process

- Selective copper reduction
 - Second step iron winning
- Focus on first step
 - **Selectivity, Efficiency,**
Influence of H_2 -conc.,
kinetics, ...
- Why H_2 instead of C, CH_4 or CO?
 - Fast kinetics
 - High selectivity



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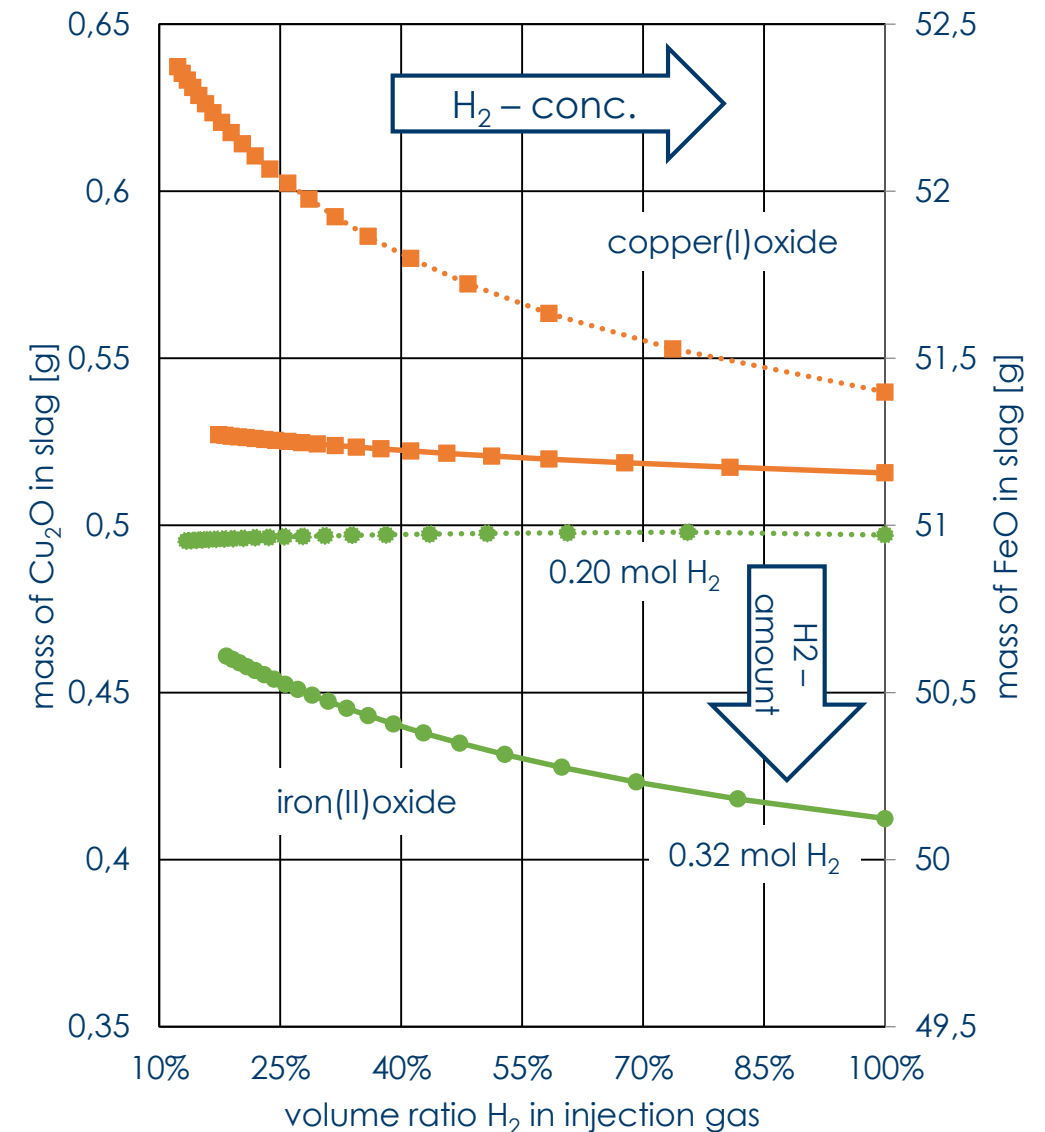
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Thermochemical simulation (reduction)

- Higher concentration of reduction gas lowers Cu_2X content
- Barrier at around 0.52 wt.% Cu_2X
- Low hydrogen amounts don't reduce iron(II)oxide
- Hydrogen yield between 28.8 – 36.9 %
 - Lowers with an increase in H_2 concentration



Simulations done with FactSage™ 8.0



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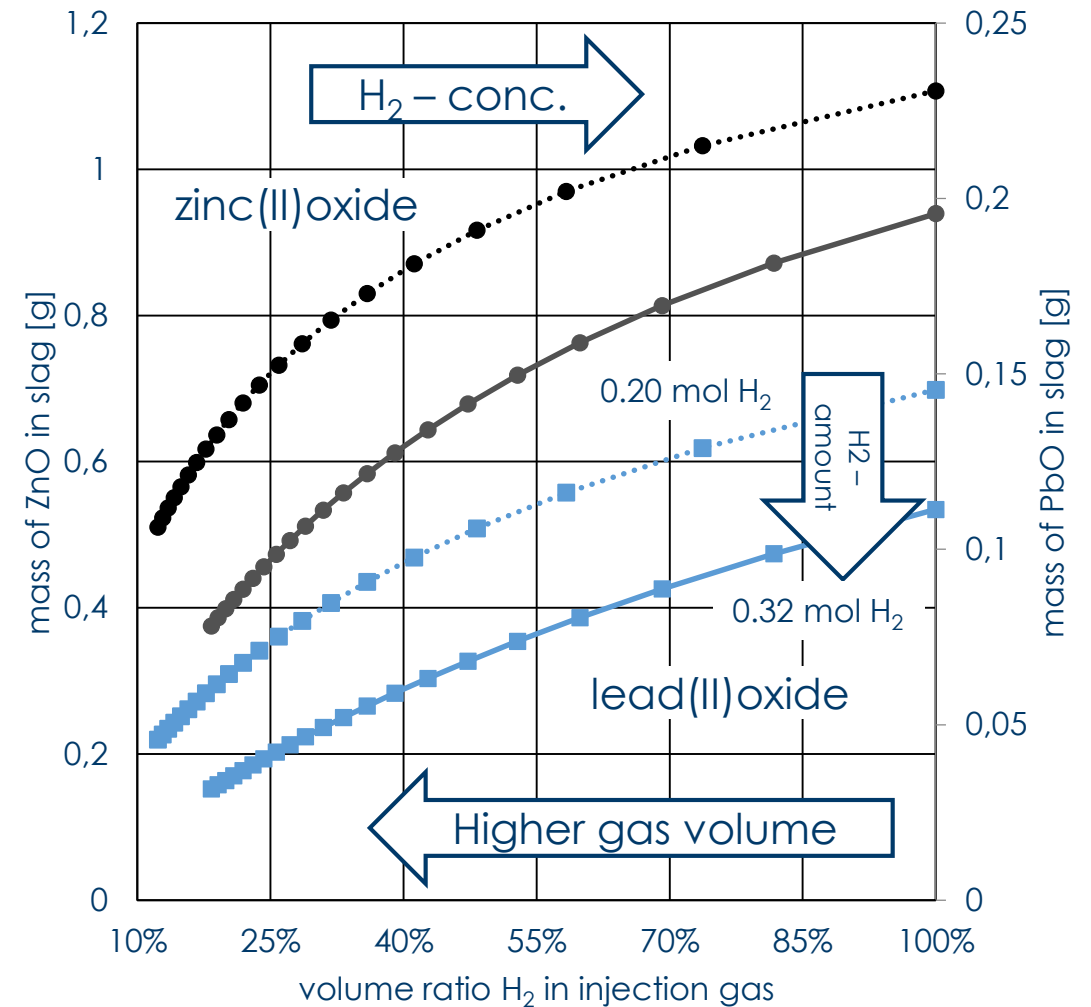
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Thermochemical simulation (fuming)

- Fuming of slags possible
 - Achieving $\sum(\text{Zn}+\text{Pb}) < 0.5 \text{ wt.}\%$ with $0.32 \text{ mol H}_2/100 \text{ g slag}$
 - Higher gas volume increases fuming effect
 - Lowering Zinc and lead with low iron reduction
- Simulation confirms idea of selective reduction



$$\text{vol. \%}_{\text{H}_2} = \frac{V_{\text{H}_2}}{V_{\text{H}_2} + V_{\text{N}_2}}$$

Simulations done with FactSage™ 8.0



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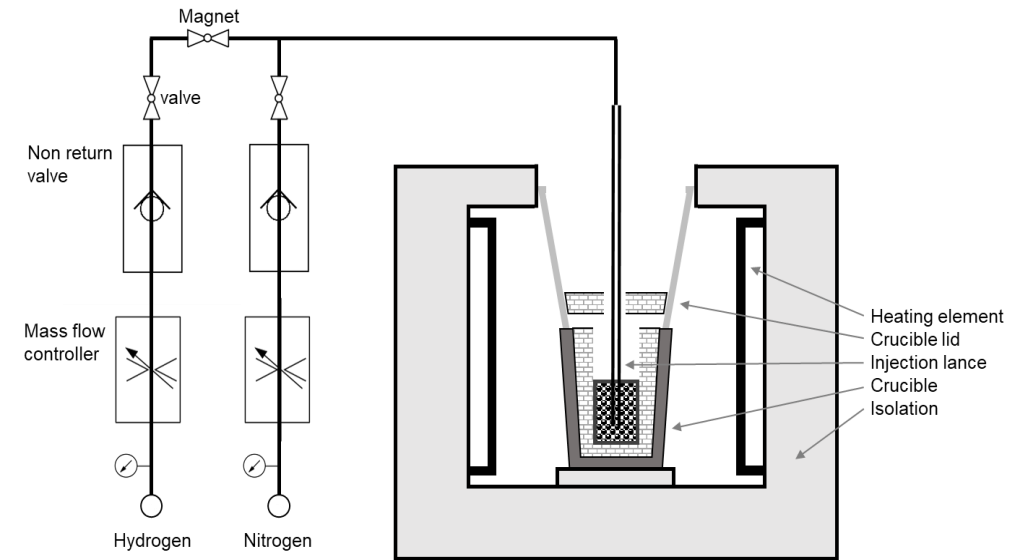
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Setup and material

- Resistant heated furnace
- Gas mixing box with mass flow controllers
- $\text{Al}_2\text{O}_3\text{-Cr}_2\text{O}_3$ -lining in crucible
- Al_2O_3 based lances
- Slag temperature $\sim 1300^\circ\text{C}$
- Two samples taken at $\frac{1}{2}$ and full H_2 amount



Wt.%	FeO	SiO ₂	Al ₂ O ₃	CaO	Cu	Mo	PbO	ZnO	S	rest
Slag 1	50.1	31.8	4.5	2.2	1.4	0.6	0.3	1.3	0.4	5.4
Slag 2	50.1	33.9	4.1	2.2	1.3	0.3	0.2	0.7	0.3	4.7



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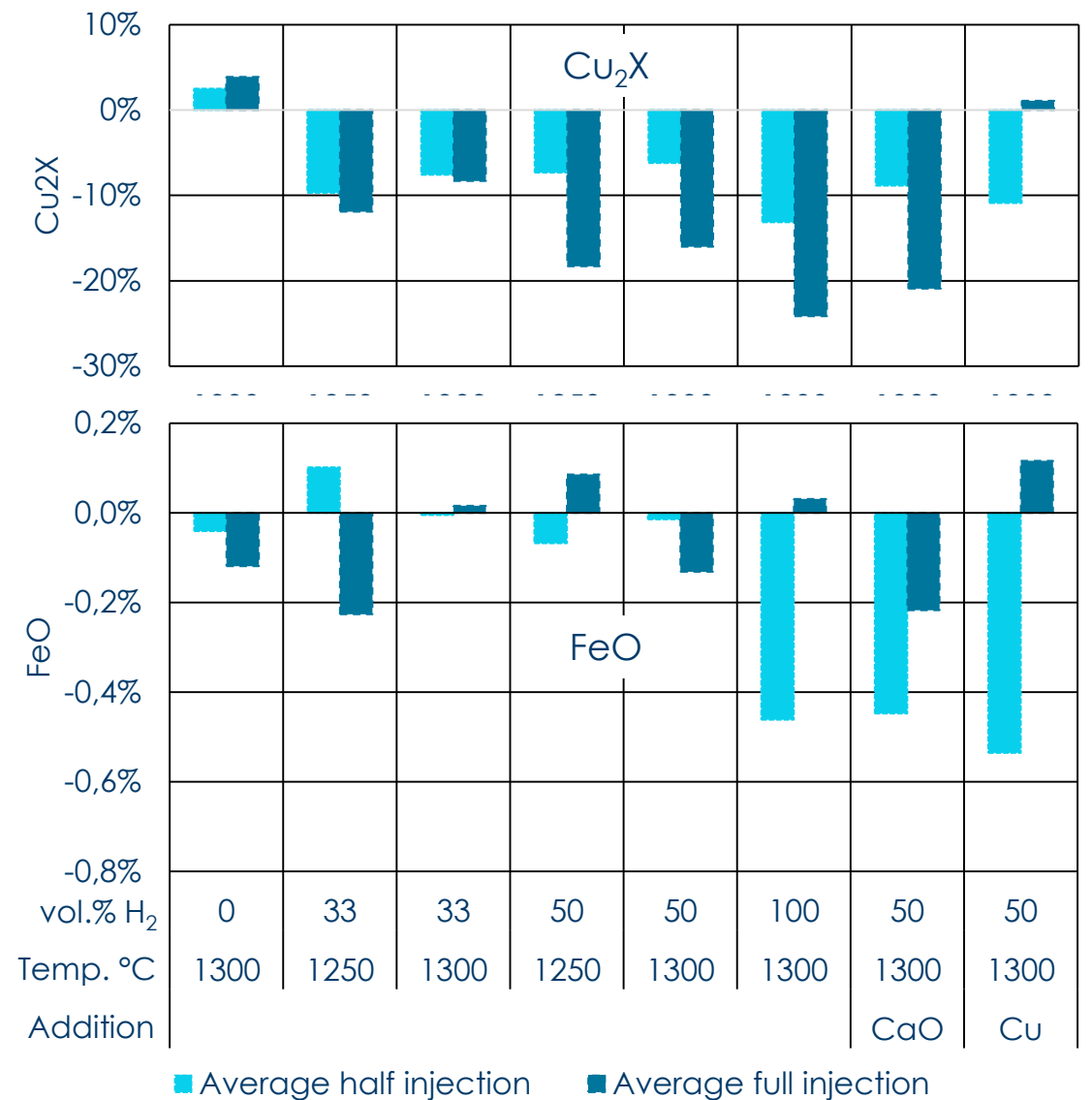
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Experimental results (reduction)

- Higher H_2 concentration leads to higher Cu_2X reduction
 - (max 24.2 %, 1.09 wt.% - starting 1.52 wt.%)
- 100 % H_2 in reduction gas leads to iron reduction
- Lime increases the reduction yield of Cu_2X

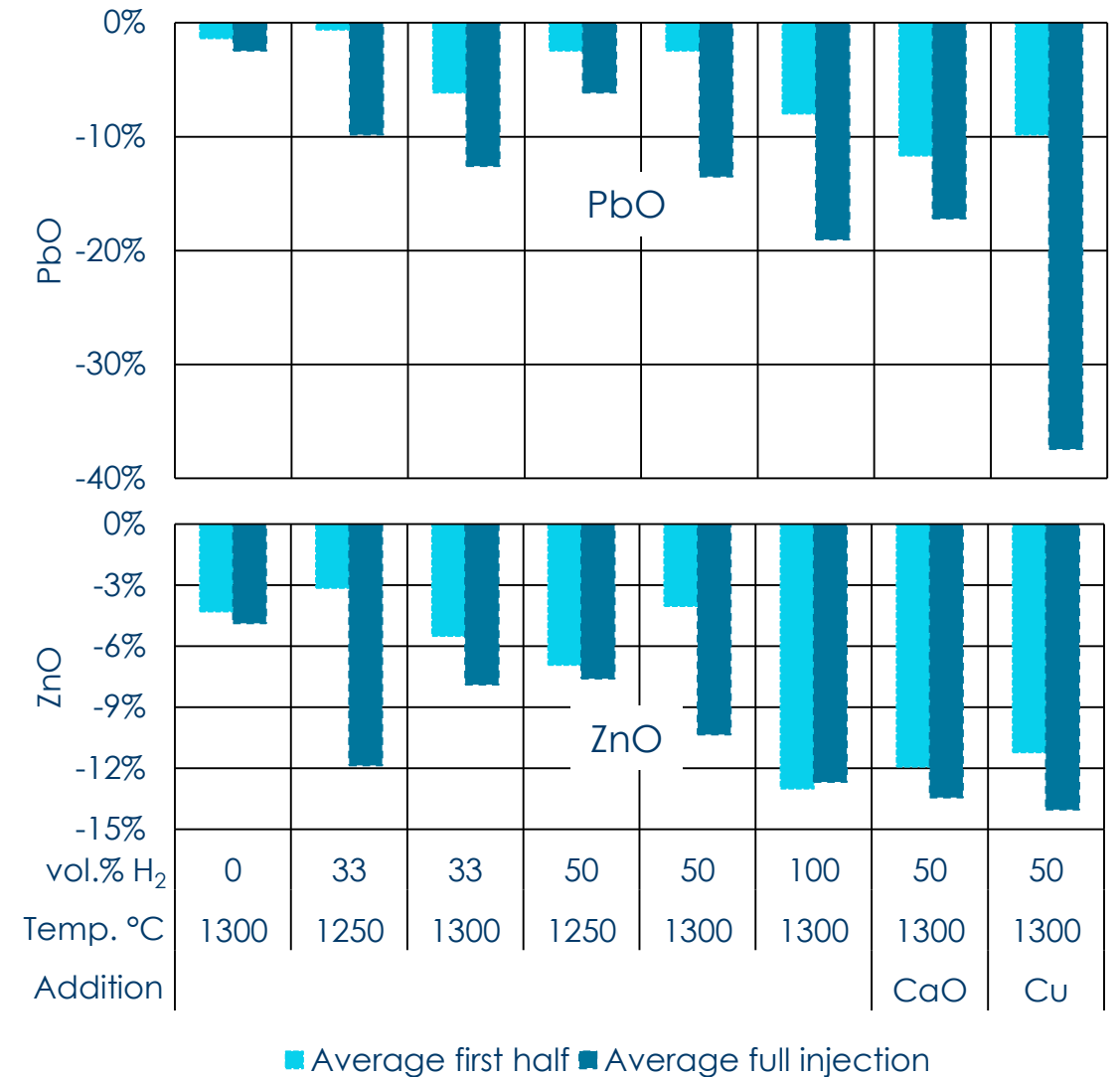


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Experimental results (fuming)

- Lead reduction similar to copper
- Zinc fuming possible with various H_2 -concentrations
- Influence of volume from simulation can not be confirmed
 - High fuming yield with high hydrogen concentration



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Efficiency of hydrogen reduction

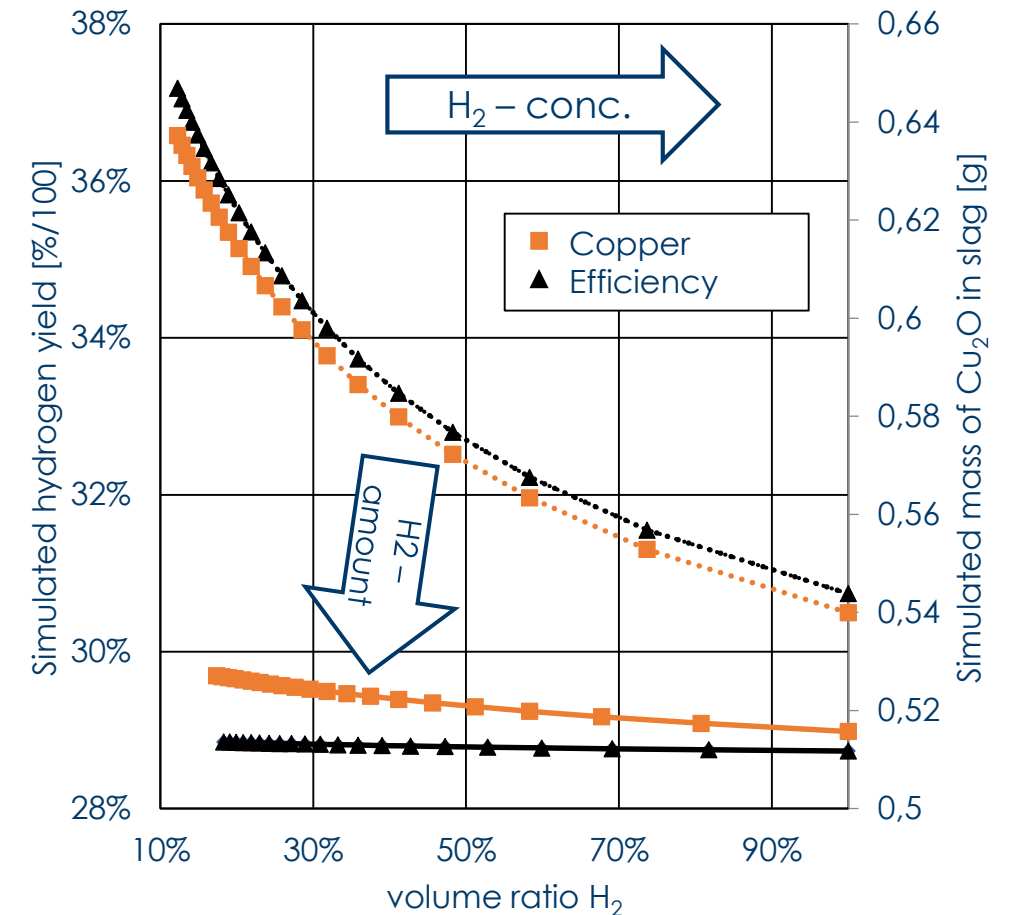
- Efficiency of FactSage™: 29 - 37 %
 - Strongly depends on Cu-content
- Experimental efficiency: 10 – 17 %
 - 27 to 58 % of simulations in small scale
 - ❖ < 10 cm slag column for reaction
- Trials with higher H₂-amount cause low efficiency

simulation:

$$\eta_{H_2} = \frac{H_{2O_{product}}}{H_{2_{injected}}}$$

experimental:

$$\eta_{H_2} = \frac{\sum Cu, Fe, Pb, Zn_{reduced}}{H_{2_{injected}}}$$



Simulations done with FactSage™ 8.0



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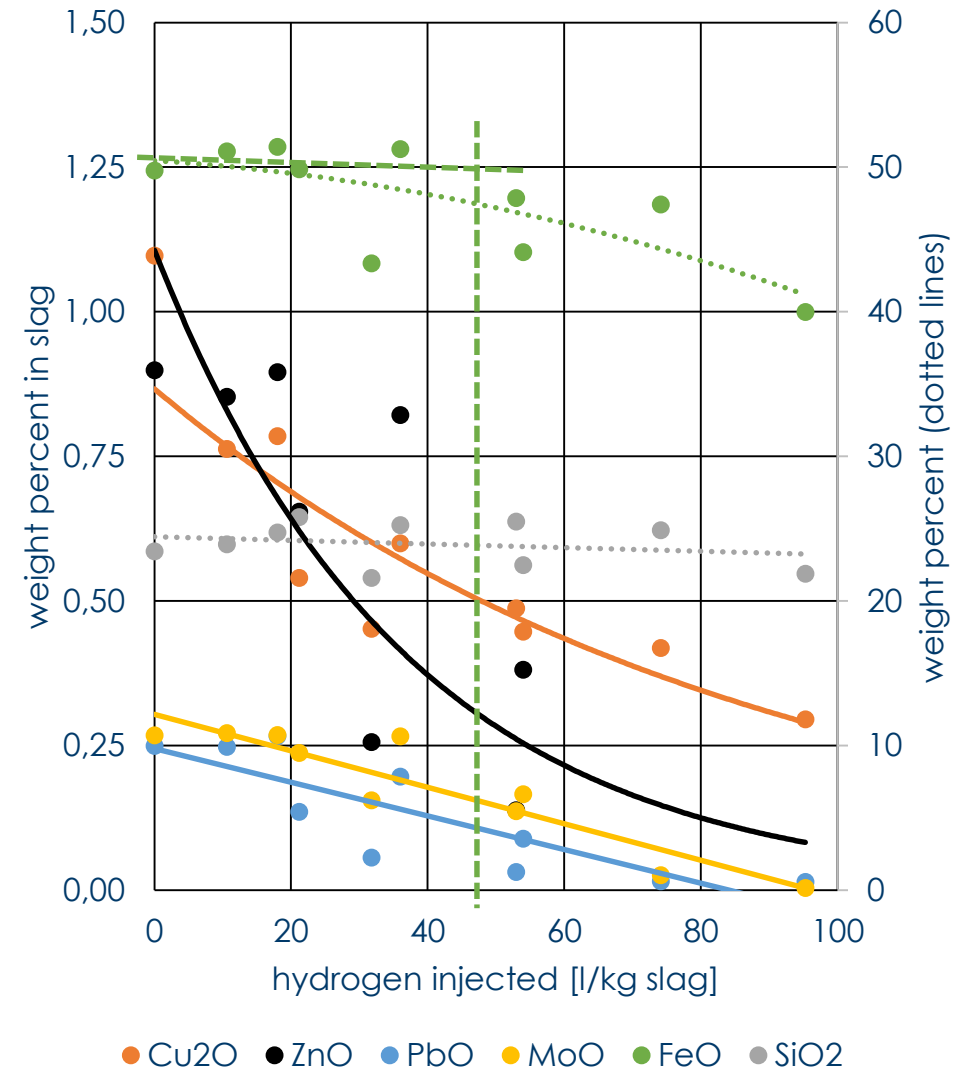
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Evaluated trials chemical analysis

- Copper decreased to 0.5 wt.% Cu₂O
 - With low FeO reduction
- Lead and zinc decrease to $\Sigma < 0.2$ wt.%
 - White and yellow powder in flue dust
- ~10 g metal/kg slag
 - <60 % Cu, 25 % Fe
 - Weight percents of Sb, Mo, Ni, As, Sn

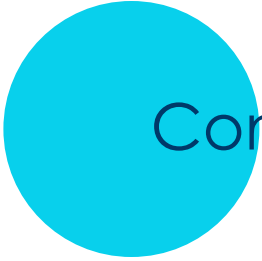


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Conclusion

- Selective reduction possible
 - > 0.5 wt.% Cu₂O
 - Max. 73 % Cu-reduction
- Hydrogen yields 10 – 17 % in lab scale
 - Low melt column and residence time
- Fuming of slags possible to low contents of ZnO and PbO < Σ 0.1 wt.%

Outlook

- Influence of H₂-concentration
- Influence of lime addition
- Kinetics of hydrogen reduction
- Upscaling of trials to 300 kg (40 cm slag column)
 - 4 t at Aurubis AG Hamburg (70 cm slag column)

Further publications

- Slag valorization symposium 2023, Belgium
- European metallurgical conference 2023, Germany



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Thank you

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